

# *Principles of Biomass Gasification*

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# What is Biomass Gasification

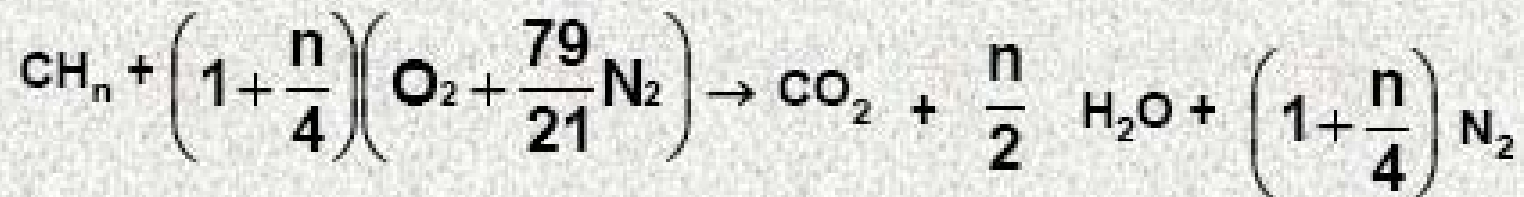
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- Conversion of Solid biomass to a gaseous fuel through thermal route
- Biomass contains carbon, hydrogen, oxygen, and small quantities of other elements
- On combustion with air  $\text{CO}_2$  and  $\text{H}_2\text{O}$  are generated
- With sub-stoichiometric combustion (limited supply of air) products like  $\text{CO}$  and  $\text{H}_2$  can be generated.
- The gas, thus generated is called producer gas

# Air-to-fuel ratio

The amount of air needed to completely burn the fuel to  $\text{CO}_2$  and  $\text{H}_2\text{O}$  is known as stoichiometric ratio. The amount required for converting carbon to carbon dioxide, hydrogen to water constitute the amount of air required. If the fuel has some oxygen in its structure then the amount of air required is smaller.

For a typical hydrocarbon we have



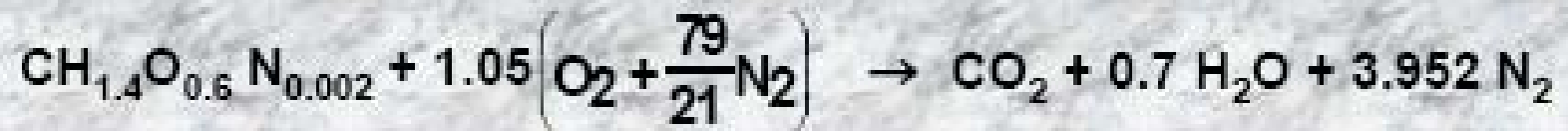
A hydrocarbon fuel leads to stoichiometric ratio (S)

$$s = \left\{ (32 + 3.7628) \left(1 + \frac{n}{4}\right) \right\} / (12 + n)$$

is 14.4 for  $n = 1.8$  and 17.1 for  $n = 4$

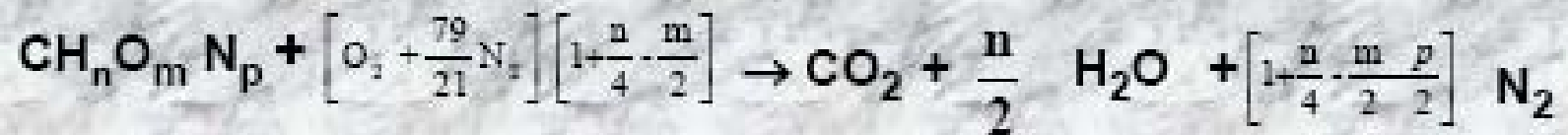
These are the typical values for diesel/gasoline and methane, [ $n = 4$ ]

If we take a typical biomass



We get  $s = 6.3$

In general



$$\frac{A}{F} = \frac{(32 + 3.7628) \left[ 1 + \frac{n}{4} - \frac{m}{2} \right]}{12 + n + 16m}$$

	n	m	Ash (%wt)	(A/F) stoichiometry
Rice husk	1.78	0.56	20.0	5.60
Saw dust	1.65	0.69	0.80	5.90
Paper	1.60	0.65	6.00	5.75
Rice straw	1.56	0.50	20.0	5.80
Douglas fir	1.45	0.60	0.80	6.30
Beech, Poplar, Red wood	1.33	0.60	0.20	6.00
Pine bark	1.33	0.60	2.90	5.85

Depending on the mixture ratio (air-to-fuel), whether it is more or less than the stoichiometric value, one has lean or rich operating conditions.

These are described by a quantity called the equivalence ratio ( $f$ ) which is the ratio of the air-to-fuel at stoichiometry to the actual value.

# Gasification?

## Combustion vs. Gasification

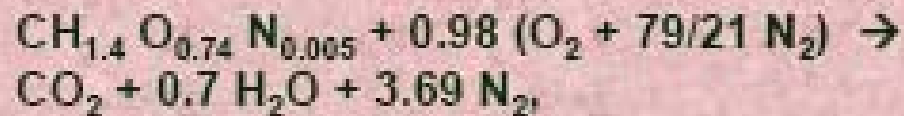
### What is Gasification?

Sub-stoichiometric combustion of fuel with oxidant; it is not simply pyrolysis of the fuel elements; it is stoichiometric combustion (oxidation) + reduction reaction leading to typical products - Hydrogen, Carbon monoxide, Methane, Carbon dioxide, some HHC, water vapour and rest Nitrogen - in proportions depending on the feed stock and reactant used.

Most biomass + Air = 20% ± 2 H<sub>2</sub>, 20% ± 2 CO, 2% CH<sub>4</sub>, 12% ± 2 CO<sub>2</sub>, 8% ± 2 H<sub>2</sub>O, rest N<sub>2</sub>.

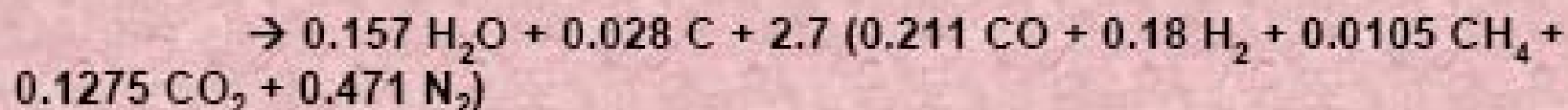
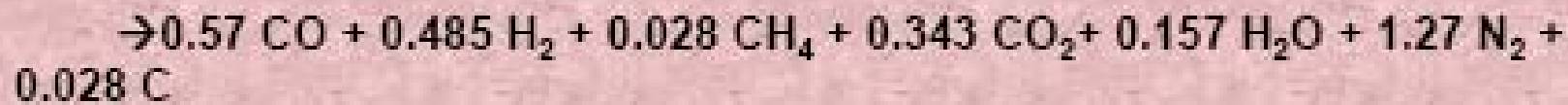
Most biomass with water vapour with added heat from external sources → 55-65 % H<sub>2</sub>, 25 - 30 % CO, rest HHC.

## Combustion



$$A/F = 5.25$$

## Gasification

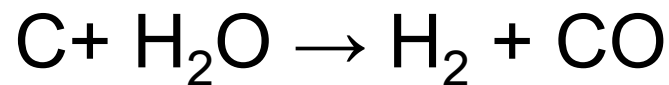
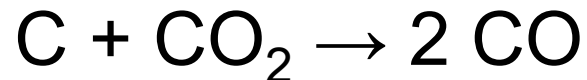


$$A/F \cong 1.805; \text{Hot gas/Fuel} = 2.805; \text{Cold gas/Fuel} \cong 2.62$$

## Steps in Gasification

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- Heating of biomass and release of volatile matter from biomass
- Combustion of volatile matter with air
- Reduction of combustion products ( $\text{CO}_2$  and  $\text{H}_2\text{O}$ ) with carbon to  $\text{CO}$  and  $\text{H}_2$





# The Gasification Process

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- Biomass when heated loses volatiles leaving fixed carbon (about 20–25 %)
- The volatile matter reacts with air providing energy for biomass heating and to raise the temperature of gases to about 1200–1400°C.
- The hot gases thus produced, which contains CO<sub>2</sub> and H<sub>2</sub>O react further with the fixed carbon to generate CO and H<sub>2</sub>.
- These are endothermic reduction reactions and bring down the temperature to about 600–700°C.
- The IISc open top reactor has a second stage of oxidation-reduction process to minimize the tar in the product gases and to improve the carbon conversion.

# Composition of Producer Gas

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- The producer gas contains CO, H<sub>2</sub>, CH<sub>4</sub>, CO<sub>2</sub>, H<sub>2</sub>O and N<sub>2</sub> with the composition given in the table

CO	18–20 %
H <sub>2</sub>	18–20 %
CH <sub>4</sub>	1–2 %
CO <sub>2</sub>	11–12 %
N <sub>2</sub>	Rest

# Impurities in the gas

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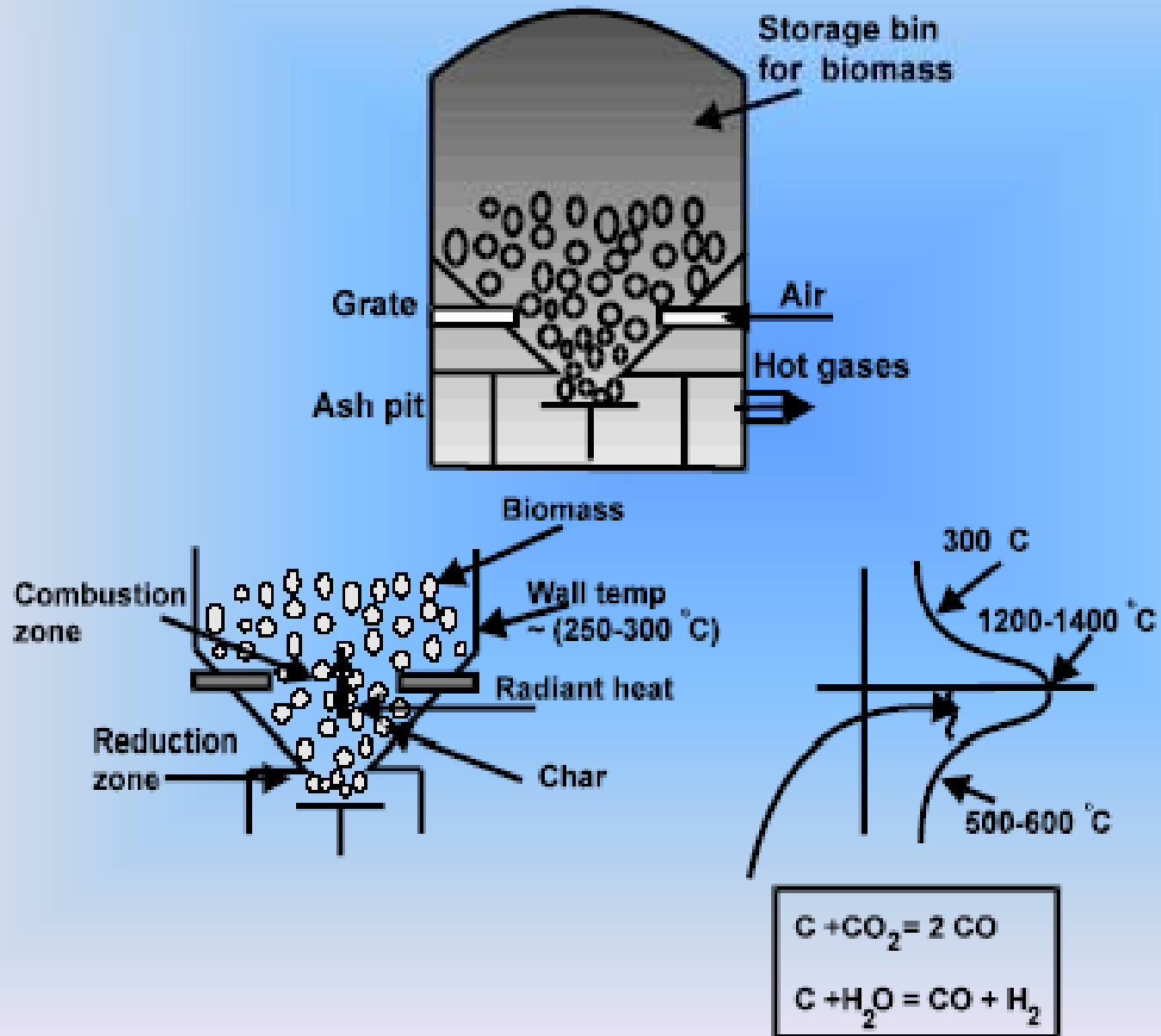
- Tar — unconverted volatile matter
  - Gets condensed and deposited in various passages
  - Causes difficulty in engine operation. Should be brought down less than 10 ppm for satisfactory engine operation
- Dust — Carbon/ ash particles carried along with gas
  - Needs to be separated for high quality applications such as engine

# Types of gasifiers

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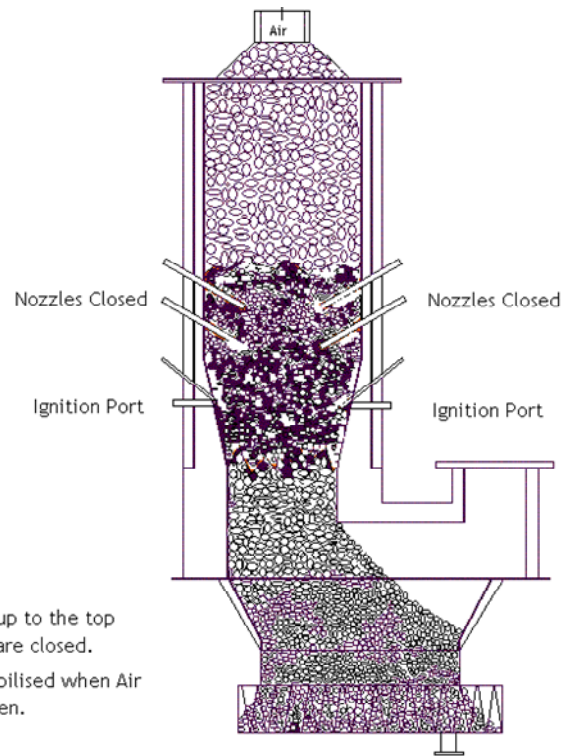
- Fixed bed
  - Up draft — high tar content in the gas
  - Down draft
    - Open top
    - Closed top
- Moving bed
  - Fluidized bed — Suitable for large installations. High tar content in the gas.
    - Bubbling
    - Circulating

## Closed top design



# Open top gasifier

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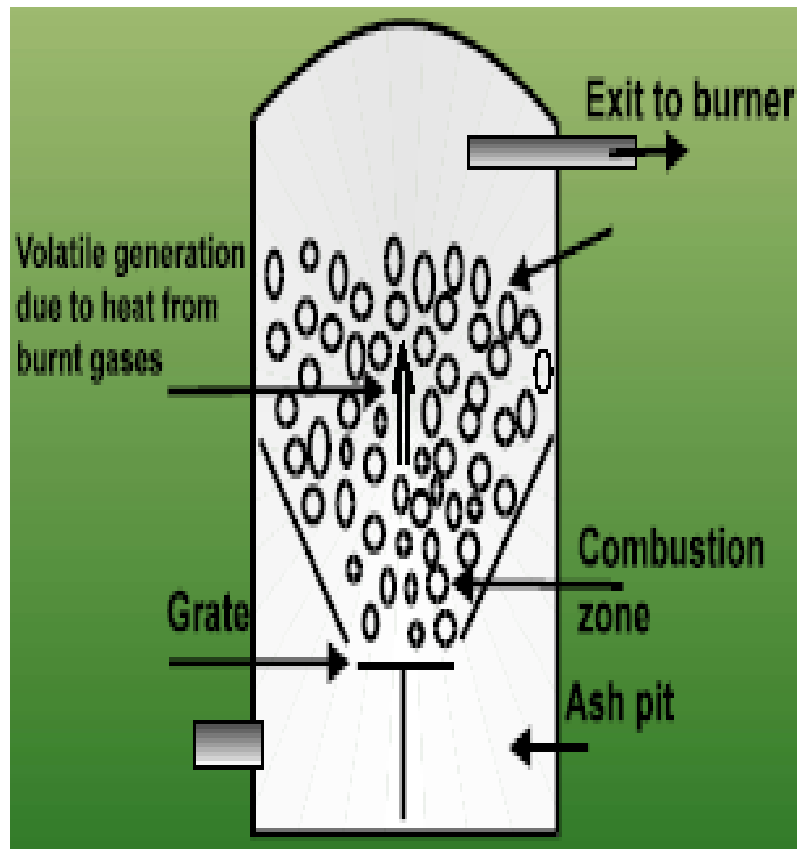


- \* Flame moves up to the top if Air nozzles are closed.
- \* Flame gets stabilised when Air nozzles are open.

# Comparison of open and closed top designs

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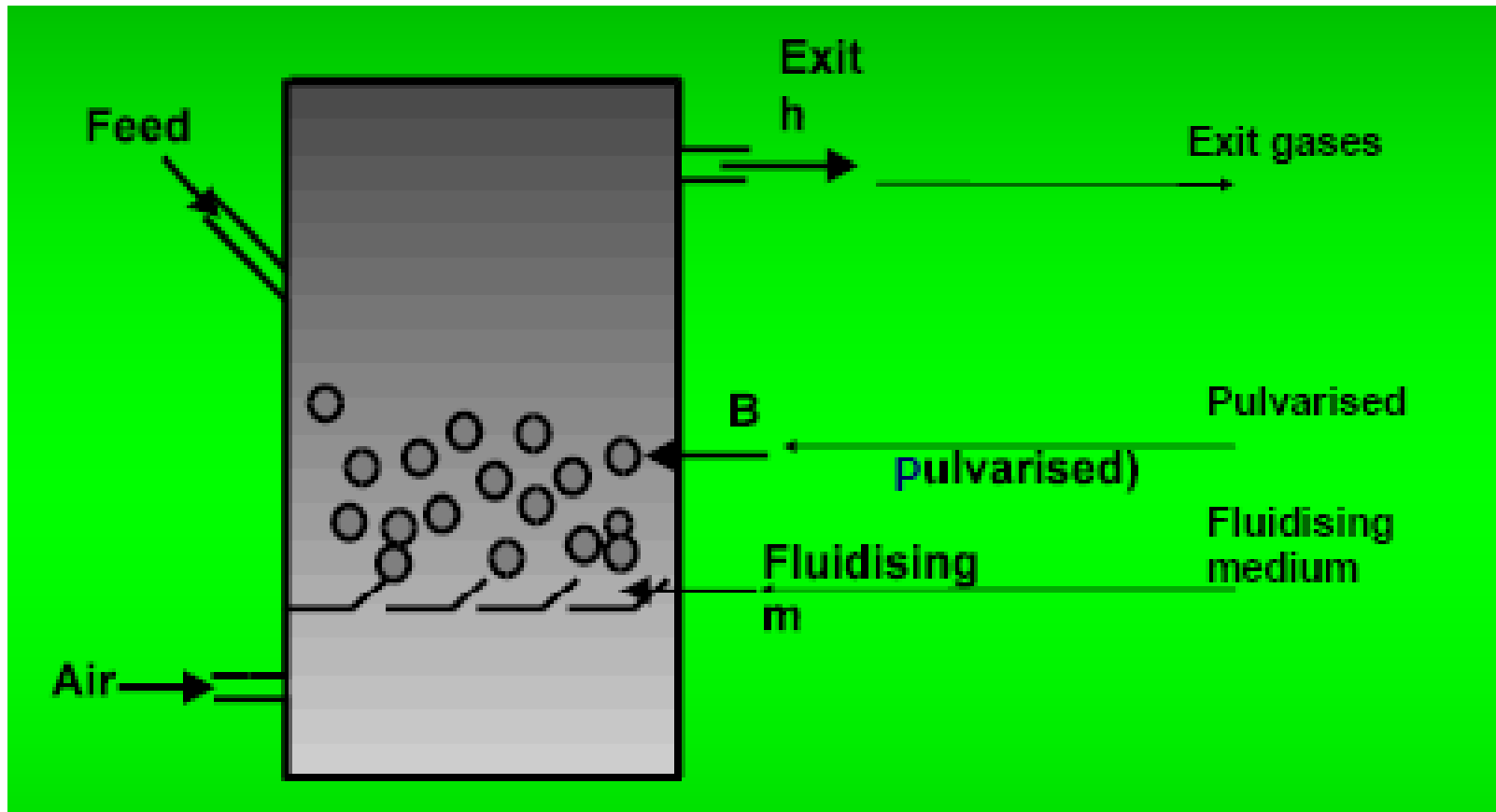
	Closed top	Open top
Nature of biomass (size)	Pieces of 20 – 100 mm depending on power level	same
Top region	Volatile matter and fuel rich conditions	Air and lean environment
Uniformity of A/F at a cross section	Non-uniform	Relatively uniform
Regions of tar rich zones	Yes	Relatively low



- **The combustible gases at the exit have a large amount of volatiles. If the combustible gases are cooled to ambient temperature, the tar in the gas condenses and leads to problems of blockage. The gas is fit for direct use in burners. This technique is useful if the downdraft kind cannot be used. It has been used for waste contaminated wood.**



# Fluidized bed gasifier



# Gas cleaning - process

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- Gas has to be cooled and cleaned for end use application  
T and P levels of 100 ppm and 1000 ppm respectively in the raw gas at 350 – 650°C
  - Cooling and cleaning is achieved by using a number of components
  - These are cyclones and cooling devices by spraying water in scrubbers
  - Further cleaning is achieved using chilled scrubbers

With this gas cleaning process it is possible to restrict the contaminants to ppb levels

# Gas cleaning

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- After cooling
  - Gas is saturated with moisture
  - Contains fine dust and condensable ( $\sim 25$  ppm) even after filtering – not acceptable to turbo charged engines
- Use the principle of condensation nuclei
  - Scrub the gas using cold water ( $< 10$  C)
    - Dries the gas by condensing the water vapor
    - This happens using the particles (Cloud Condensation Nuclei) – thus removing the particulate  $< 10^{-3}$  microns
    - The gas is dry and clean to ppb level

**Chilled scrubbers are currently being used  
in all the systems**

# Properties of Producer Gas vis-à-vis other Gaseous Fuels

Fuel + Air	Fuel LCV, MJ/kg	Air/Fuel @ ( $\Phi = 1$ )	Mixture, MJ/kg	$\Phi$ , Limit		$S_L$ (Limit), cm/s		$S_L$ $\Phi = 1$ , cm/s	Peak Flame Temp, K	Product/Reactant Mole Ratio
				Lean	Rich	Lean	Rich			
H <sub>2</sub>	121	34.4	3.41	0.01	7.17	65	75	270	2400	0.67
CO	10.2	2.46	2.92	0.34	6.80	12	23	45	2400	0.67
CH <sub>4</sub>	50.2	17.2	2.76	0.54	1.69	2.5	14	35	2210	1.00
C <sub>3</sub> H <sub>8</sub>	46.5	15.6	2.80	0.52	2.26	-	-	44	2250	1.17
C <sub>4</sub> H <sub>10</sub>	45.5	15.4	2.77	0.59	2.63	-	-	44	2250	1.20
PG	5.00	1.35	2.12	0.47 a	1.60 b	10.3	12	50 c	1800 d	0.87

PG: H<sub>2</sub> - 20%, CO - 20%, CH<sub>4</sub> - 2%; a:  $\pm 0.01$ , b:  $\pm 0.05$ , c:  $\pm 5.0$ , d:  $\pm 50$  ;

# Applications of Gasification Process

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Process that converts solid fuel to gaseous fuel

- Used in an internal combustion engine for power generation to substitute fossil fuel
  - Diesel engine – for dual fuel application
  - Gas engine – for single fuel
- Used in heat application
  - Low temperature – drying, etc
  - High temperature – furnaces, kilns, etc

# Biomass for Gasification

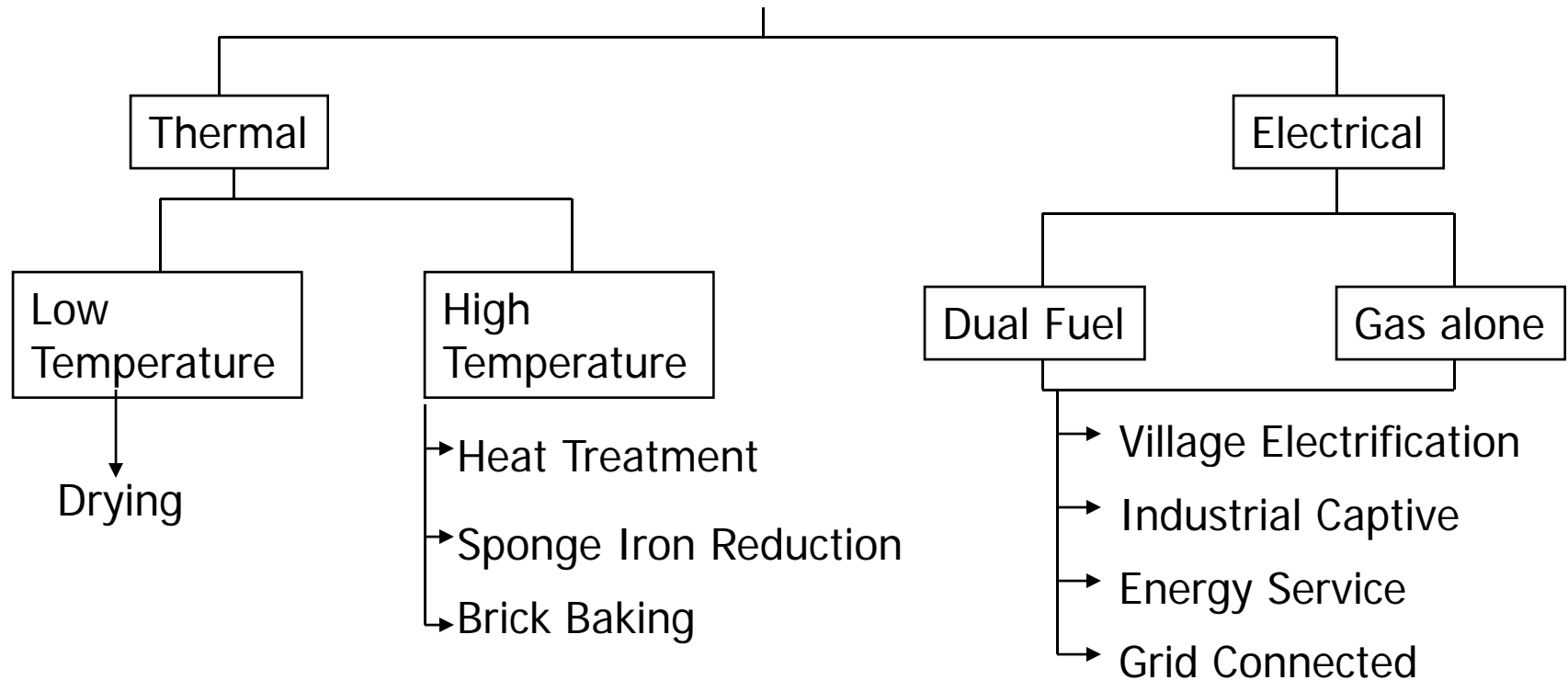
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# Applications Serviced

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## Gasifier



# Summary of gasification

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- **Gasifiers are devices which convert solid biomass into gaseous fuels for combustion in furnaces or in engines**
- **Gasifiers give a precise control of instantaneous power some thing not possible in combustors (for solid fuel)**
- **Woody biomass gasifiers are of down draft, updraft types  
Downdraft gasifiers can be either closed or open top**
- **For engine applications downdraft gasifier is the most suitable. For engine applications involving variable load/ power demand, open top downdraft gasifiers are most suitable.**
- **Updraft gasifiers may be the most appropriate if the biomass is contaminated, unsized and of a variety of shapes making downdraft gasification difficult. The applications are only thermal.**